Design of Covalent Organic Frameworks for Methane Storage

Jose L. Mendoza-Cortes, Tod A. Pascal, and William A. Goddard, III*

Materials and Process Simulation Center (MC 139-74), California Institute of Technology, Pasadena, California 91125, United States

ABSTRACT: We designed 14 new covalent organic frameworks (COFs), which are expected to adsorb large amounts of methane (CH₄) at 298 K and up to 300 bar. We have calculated their delivery uptake using grand canonical Monte Carlo (GCMC) simulations. We also report their thermodynamic stability based on 7.5 ns molecular dynamics simulations. Two new frameworks, COF-103-Eth-trans and COF-102-Ant, are found to exceed the DOE target of 180 v/(STP)/v at 35 bar for methane storage. Their performance is comparable to the best previously reported materials: PCN-14 and Ni-MOF-74. Our results indicate that using thin vinyl bridging groups aid performance by minimizing the interaction methane-COF at low pressure. This is a new feature that can be used to enhance loading in addition to the common practice of adding extra fused benzene rings. Most importantly, this report shows that pure nonbonding interactions, van der Waals (vdW) and electrostatic forces in light elements (C, O, B, H, and Si), can rival the enhancement in uptake obtained for microporous materials derived from early transition metals.

1. INTRODUCTION

Crystalline microporous materials systems such as the metal–organic frameworks (MOF) and covalent organic frameworks (COF) are valuable for trapping enormous amounts of gases such as H₂, CO₂, and CH₄ at modest pressures, due to their outstanding porosity. Thus COF-105 has a surface area of 6450 m²/g (equivalent to 1.4 American football fields per gram) and COF-108 has a pore volume of 5.4 cm³/g with the lowest density crystalline material known (0.17 g/cm³). We are interested in COFs because they contain light elements (B, C, O, H, and Si). Such materials could be useful in automotive applications (storing CH₄ rather than gasoline) and in CH₄ capture to prevent this greenhouse gas for getting into the atmosphere, of critical importance because methane is 21 times more effective in trapping heat in the atmosphere than CO₂.

We are also interested in the delivery amount of gas rather than the excess uptake because delivery is more important for industrial application. We define the delivery amount as the difference in the total amount adsorbed at certain pressure compared to the base pressure of the system, for example, atmospheric pressure. Much effort has been focused on reaching the DOE target of storing methane at 35 bar, because this is the pressure in natural gas pipelines. However, current commercial tanks can now hold pressures up to 250 bar, and hence we are interested in which frameworks are useful in this pressure range. Here we use virtual screening of candidate materials to discover new designs for COFs that can produce better CH₄ delivery methane uptake than current materials.

Our previous results showed that small pore diameter plus a high content of accessible aromatic rings give a heat of adsorption (Qₑ) suitable for binding CH₄ at 298 K. On the other hand, too low a pore diameter leads to quick saturation at low pressures, as was found for COF-1. We also found that methane–methane interactions are important in achieving good sorption performance with increasing pressure. On the basis of these lessons, we designed 15 new COFs containing alkyl substituents that we expected to take advantage of these interactions.

We based the new designs on building blocks with a 3,4-connectivity, shown previously to yield carbon–nitride (ctn) and boracite (bor) topologies. Figure 1 shows the building block used for this study as well as the chemistry of the condensation reactions. Scheme 1 summarizes the topologies and the kind of substituents used for the frameworks.

This paper is organized as follows. Section 2 describes the details about the methodology used for each simulation. It also includes the criteria used for the topological design of the new COFs. Section 3 presents the results about the volumetric delivery performances as well as Qₑ values of our compounds versus representatives COFs and MOFs without open metal sites (COF-102, COF-103, COF-105, COF-108, COF-202, MOF-177, and MOF-200). We also discussed the comparison of our results with previous studies. Finally, section 4 summarizes our main findings.

2. METHODOLOGY

2.1. Force Field. Nonbonding terms. Previously we developed a force field for nonbonded interactions (vdW-FF) of COFs and CH₄ based on quantum mechanics (QM) calculations at the MP2-IR/QZVPP level expected to be accurate for London dispersion forces (van der Waals attraction). We validated this
FF with the CH₄ equation of state at various temperatures (260–400 K) and pressures (1, 10, and 100 bar) and with experimental loading curves. This vdW-FF was used to calculate the loading curves.

Covalent Terms. For this work we are interested in studying the stability of the frameworks using molecular dynamics (MD). Thus we have combined our vdW-FF with the covalent terms from the DREIDING force field for use in the MD studies.

2.2. Electrostatic Interactions. We described the electrostatic interactions using used the Mulliken charges from QM for the CH₄ molecule (C, -0.43820; H, +0.10955) and the QEq (charges equilibration) charges for the framework. 18

2.3. Grand Canonical Monte Carlo. We used grand canonical Monte Carlo (GCMC) simulations to calculate the loading curves for these frameworks. Here we use our vdW-FF with QEq charges for the framework and QM charges for the CH₄. At each pressure we considered 3 000 000 GCMC steps and tested that convergence was attained in each simulation. Every GCMC step allows four possible events: translation, rotation, creation, and annihilation each at equal probability. 19,20 We used the GCMC code as implemented in Cerius2.

2.4. Molecular Dynamics. To test the stability of the compounds, we performed molecular dynamics (MD) simulations using the LAMMPS simulation engine with a 1 fs time step. 21 We used the combined force field (vdW-FF plus Dreiding) to treat the interactions. The long-range electrostatics were treated using the particle–particle particle-mesh Ewald technique, with a real space cutoff of 10 Å and an accuracy tolerance of 10⁻⁶. For each MD simulation we started with the equilibrium geometry from 300 steps of conjugated gradient (CG) minimization (cell coordinates and atom positions) followed by 10 ps of NVT dynamics to heat the system from 10 to 298 K. Finally, we ran NPT dynamics at 1 atm and 298 K for 7.5 ns from which we collect all relevant data. The temperature damping constant was 0.1 ps, and the pressure damping constant was 2.0 ps. The equations of motion used are those of Shinoda et al., 23 which combine the hydrostatic equations of Martyna et al., 24 with the strain energy proposed by Parrinello and Rahman. 25 The time integration schemes closely follow the time-reversible measure-preserving Verlet integrators derived by Tuckerman et al. 26

2.5. Topological Consideration in the Design of COFs. For the design of the 3,4 frameworks we used only the ctn (I43d space group) and bor (P4₃m space group) topologies because they have been shown to be the most stable. 9,15,16 To build each structure, we used the corresponding space group and add the irreducible representation of the ligand into it. None of the ligands produces lower symmetry frameworks.

We minimize these frameworks with CG for 500 steps, which always led to convergence. During the design of COF-102-Eth-trans, COF-103-Eth-trans, and COF-105-Eth-trans, we found that the cis version is incompatible with these constraints and that the framework is unstable after minimization, leaving the trans isomer as the only choice. The optimized structures coordinates are reported in the Supporting Information.

3. RESULTS AND DISCUSSION

3.1. Delivery Volumetric Uptake in Designed COFs. The DOE goal for methane storage is 180 v(STP)/v at 35 bar. Here, v(STP)/v denotes the volume of methane per volume of system, where STP is the standard temperature and pressure of 298 K and 1.01 bar. 27 Only two materials have been reported to satisfy the methane uptake DOE requirements at 35 bar: Ni-MOF-74 and PCN-14. In the experimental reports, 1 atm and 273 K were used as the standard units. Thus, Ni-MOF-74 reached 190 excess v(273 K, 1 atm)/v and PCN-14 reached 220 excess v(273 K, 1 atm)/v, the latter measured at 290 K. To make a fair comparison in the following discussions, we multiply these experimental quantities by 1.09 (or 298/273) to get our defined STP. Therefore, after conversion, we obtain 207 v(STP)/v for and Ni-MOF-74 and 240 v(STP)/v for PCN-14.

The representative MOF-177, which is now in industrial production for automotive applications, achieves only 91
The Journal of Physical Chemistry A

ARTICLE

The Journal of Physical Chemistry A

The Journal of Physical Chemistry A

The Journal of Physical Chemistry A

use the experimental QSTP have converted the experimental uptake (273 K, 1 atm) to our framework. We use only experimental uptakes for PCN-fi summarized in Table 1, where we used standard de

QSTP excess v(Ch4) at 35 bar. The excess and total uptakes are summarized in Table 1, where we used standard definitions for these quantities. We use only experimental uptakes for PCN-14 and Ni-MOF-74 because our vdW-FF does not deal yet with open metal sites.

The results for the delivery amount of methane for our four best new designs for up to 35 bar are shown in Figure 2, whereas the performance for the remaining 11 systems is in the Supporting Information. At 35 bar (in v(STP)/v delivery units) the best performers are

- COF-103-Eth-trans (192 ± 4), exceeding the DOE target,
- COF-102-Ant (180 ± 3),
- COF-102-Eth-trans (172 ± 3), and
- COF-105-Eth-trans (110 ± 2).

Thus COF-103-Eth-trans stores 5.6 times as much as bulk CH4 at the same pressure (bulk CH4 reaches 34 ± 1). All our designed COFs have superior performance to previously reported COFs and MOFs, such as COF-102 (137 ± 3), MOF-177 (112 ± 2), and MOF-200 (81 ± 2).

The new materials were designed for best performance at 35 bar. At higher pressures, the trend in performance (at 300 bar and in v(STP)/v delivery units) changes:

- COF-105-Eth-trans (350 ± 7),
- COF-103-Eth-trans (328 ± 7),
- COF-102-Eth-trans (306 ± 6), and
- COF-103-Ant (258 ± 5).

Therefore, at 300 bar, COF-105-Eth-trans stores 1.3 times as much as an empty container (bulk CH4 takes 263 ± 3). Other good performers over the range of 1–300 bar are shown in the Supporting Information. For example, at 300 bar, COF-103 reaches 352 ± 7 delivery v(STP)/v, followed by COF-105 (327 ± 7), COF-108 (318 ± 6), COF-212 (310 ± 6), COF-105-Met-Met (308 ± 6), and COF-108-Met-Met (302 ± 6). We see that some of these new designs perform better than the archetypal frameworks: COF-102 (340 ± 7), MOF-177 (336 ± 7), and MOF-200 (321 ± 6). Figure 2 shows that COF-102-Ant performs comparable to bulk CH4 container at 300 bar whereas under 35 bar it approaches the DOE target.

Our results show that attaching alkyl substituents such as –CH3, –CH2CH3, –CH2CH2CH3, –CH2(CH3)2, –C(CH3)3, or –(CH2)3CH3 to the benzene rings does not increase the binding over having the simple H substituent. Among alkyl-substituted benzenes, the type of isomer matters because the one with higher surface area performs better, in particular when propyl (2590 m2/g) and isopropyl (1420 m2/g) are compared. The propyl substituent has a higher uptake when compared to isopropyl because more atoms are available to interact with a sorbent molecule and gives higher surface area even though they have the same components.

3.2. Isosteric Heat of Adsorption. Our calculated Qst values are shown in Figure 3. These trends can be understood from a

Figure 2. CH4 uptake for the best COF performers. The delivery amount using a base pressure of 1 bar is reported. The best performers at 35 bar are shown along with some that perform best at 300 bar. Solid lines indicate published compounds.

Table 1. Isosteric Heat of Adsorption (Qst), Surface Area (S)Pore Volume (VP), and Uptake of the Framework Series at 298 K (Where Tot = Total, Exc = Excess, and Eel = Delivery)^a

<table>
<thead>
<tr>
<th>Material</th>
<th>Qst (kJ/mol)</th>
<th>S (m²/g)</th>
<th>Vp (cm³/g⁻¹)</th>
<th>Tot CH₂⁺ [v(STP)/v] at 35 bar</th>
<th>Exc CH₂⁺ [v(STP)/v] at 35 bar</th>
<th>Del CH₂⁺ [v(STP)/v] at 35 bar</th>
<th>Del CH₂⁺ [v(STP)/v] at 300 bar</th>
</tr>
</thead>
<tbody>
<tr>
<td>PCN-14</td>
<td>30.0</td>
<td>1753</td>
<td>0.87</td>
<td>251a (230°)</td>
<td>196</td>
<td>145</td>
<td>150</td>
</tr>
<tr>
<td>Ni-MOF-74</td>
<td>20.2</td>
<td>1033</td>
<td>0.54</td>
<td>218a (200°)</td>
<td>120</td>
<td>80</td>
<td>150</td>
</tr>
<tr>
<td>COF-1</td>
<td>25.1</td>
<td>1230</td>
<td>0.38</td>
<td>196</td>
<td>145</td>
<td>150</td>
<td></td>
</tr>
<tr>
<td>COF-102</td>
<td>10.5</td>
<td>4940</td>
<td>1.81</td>
<td>143</td>
<td>120</td>
<td>137</td>
<td>340</td>
</tr>
<tr>
<td>COF-102-Ant</td>
<td>18.4</td>
<td>2720</td>
<td>0.75</td>
<td>215</td>
<td>200</td>
<td>180</td>
<td>258</td>
</tr>
<tr>
<td>COF-102-Eth-trans</td>
<td>13.1</td>
<td>4640</td>
<td>1.20</td>
<td>184</td>
<td>166</td>
<td>172</td>
<td>306</td>
</tr>
<tr>
<td>COF-103-Eth-trans</td>
<td>13.3</td>
<td>4920</td>
<td>1.36</td>
<td>206</td>
<td>187</td>
<td>192</td>
<td>328</td>
</tr>
<tr>
<td>COF-105-Eth-trans</td>
<td>9.3</td>
<td>6350</td>
<td>3.62</td>
<td>114</td>
<td>86</td>
<td>110</td>
<td>350</td>
</tr>
<tr>
<td>MOF-177</td>
<td>9.6</td>
<td>4800</td>
<td>1.93</td>
<td>116</td>
<td>91</td>
<td>112</td>
<td>336</td>
</tr>
<tr>
<td>MOF-200</td>
<td>7.9</td>
<td>5730</td>
<td>4.04</td>
<td>84</td>
<td>54</td>
<td>81</td>
<td>321</td>
</tr>
<tr>
<td>Pure CH₄</td>
<td>3.0</td>
<td>35</td>
<td></td>
<td>34</td>
<td></td>
<td>346</td>
<td></td>
</tr>
</tbody>
</table>

^a The st values are reported as an average from 1 to 300 bar.
comparison of COF-1, COF-102-Ant, and COF-103-Eth-trans (Table 1). COF-1 has the highest $Q_a$ among COFs, but it is saturated by 40 bar, giving the poorest delivery uptake. COF-102-Ant outperforms COF-1 despite a smaller $Q_a$ value due to the higher $S_A$ and $V_p$. Finally, COF-103-Eth-trans is the best performer due to its balance of mild $Q_a$, high $S_A$ and high $V_p$.

High $Q_a$ (>20 kJ/mol) at low pressures and low $S_A$ and $V_p$ lead to low delivery amount. The same analysis was done for PCN-14 and Ni-MOF-74 where experiments found high $Q_a$ (30.0 and 20.2 kJ/mol, respectively, at nearly 0 bar) but poor $S_A$ (1753 and 1033 m$^2$/g, respectively) and $V_p$ (0.87 and 0.54 cm$^3$/g, respectively). Thus we expect that PCN-14 and Ni-MOF-74 will saturate at 100 bar, consistent with their experimental sorption isotherm curves trend. We did not simulate PCN-14 and Ni-MOF-74 in this study because we have not yet developed a FF to deal with the open metal sites, which are an important feature in these compounds. The trends in performance at higher pressure are also shown for archetypal MOF-177 and MOF-200, which have lower $Q_a$ of 9.7 ± 0.5 and 8.0 ± 0.2, respectively. However, the higher $S_A$ (4800 and 5730 m$^2$/g, respectively) and $V_p$ (1.93 and 4.04 cm$^3$/g, respectively) give them an advantage at pressure beyond 100 bar.

In this work we are focused on getting the best performance in delivery units and this requires a low interaction methane-COF in the low-pressure range. In other words, we want to get a low $Q_a$ at low pressure. We have succeeded in obtaining this behavior for COF-102-Eth-trans and COF-103-Eth-trans by using the tiny vinyl link, as demonstrated by the shape of their $Q_a$ curves, which are similar to that of COF-102 but more marked for the entire pressure range. Eventually, methane—methane interactions compensate to show moderate $Q_a$. This is opposite to the $Q_a$ profile of COF-102-Ant where the link being used gives a high interaction at low loading (Figure 3). Therefore, our new designs using vinyl linkers present a new way to maximize delivery uptake, which is different from the approach of using fused phenyl rings.

### 3.3. Stability of COFs

Recently, it was suggested that COF-108 and even COF-102 might collapse due to instability of the frameworks; however, the same study suggested that for COF1 the “AA” conformation is more stable than the experimentally observed “AB” conformer. Therefore, we decided to study the stability of our newly designed COFs with MD simulations. Our results show that cell parameters of our new COFs change only slightly (0.130—0.142%) throughout the entire dynamics while the cell angles stayed at 90° (orthorhombic) as shown in Table 2 and Figure 4.

For comparison, we also performed MD on the characteristic MOF-5 because it is very well documented experimentally that the lattice parameters change from 25.670 to 25.910 Å over a temperature range of 3.5—300 K but remain stable under these conditions. We find that MOF-5 has a change of 0.219% in the lattice parameters, larger than our new COFs (Table 2). This indicates that our new COFs and the experimental COFs are stable without guest molecules at 298 K and 1 atm.

### 3.4. Comparisons to Previous Computational Studies

A previous computational report about sorption of CH$_4$ on MOFs showed that increasing the number of fused benzene rings increases the $Q_a$ value. However, they reported that their empirical vdW attraction terms led to errors of 5.7—9.9% greater than experiments. This study did not report the stability of their designed compound IRMOF-993, and experimentalists

![Figure 3. Heat of adsorption calculated for the compounds in Figure 2. The results for the remaining compounds are in the Supporting Information.](image)

![Figure 4. Lattice parameter variations obtained from MD for several COFs. The lattice parameters are in Angstroms (Å) and time in nanoseconds (ns). COF-103 and COF-105-Eth-trans are not shown; the statistics are summarized in Table 2.](image)

### Table 2. MD statistics for the frameworks obtained at 298 K.

<table>
<thead>
<tr>
<th>Material</th>
<th>MD lattice (Å)</th>
<th>MD std dev (%)</th>
<th>Exp lattice (Å)</th>
</tr>
</thead>
<tbody>
<tr>
<td>COF-102</td>
<td>27.444</td>
<td>0.0268 (0.098%)</td>
<td>27.177</td>
</tr>
<tr>
<td>COF-103</td>
<td>27.860</td>
<td>0.0280 (0.101%)</td>
<td>28.248</td>
</tr>
<tr>
<td>COF-108</td>
<td>28.917</td>
<td>0.0402 (0.139%)</td>
<td>28.401</td>
</tr>
<tr>
<td>COF-102-Ant</td>
<td>27.759</td>
<td>0.0389 (0.140%)</td>
<td></td>
</tr>
<tr>
<td>COF-102-Eth-trans</td>
<td>19.820</td>
<td>0.0274 (0.138%)</td>
<td></td>
</tr>
<tr>
<td>COF-103-Eth-trans</td>
<td>20.371</td>
<td>0.0290 (0.142%)</td>
<td></td>
</tr>
<tr>
<td>COF-105-Eth-trans</td>
<td>37.043</td>
<td>0.0483 (0.130%)</td>
<td></td>
</tr>
<tr>
<td>MOF-5</td>
<td>24.286</td>
<td>0.0533 (0.219%)</td>
<td>25.790 (0.46%)</td>
</tr>
</tbody>
</table>

*The standard deviation was calculated after 10 ps. All these frameworks have a cubic lattice. The experimental lattice value for MOF-5 is taken as the median of most representative experimental conditions reported (the average for these experiments is 25.833 Å). For comparison we show in parentheses the percentage from upper and bottom bounds.*

34—36
The U.S. Department of Energy. The computer facilities of the Materials and Process Simulation Center were supported by ONR-DURIP and ARO-DURIP.

**REFERENCES**


